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OCT 31 2006

AMENDMENTS
In the Claims

Status of Claims

- 1 1.(currently amended) An apparatus for condensing multi-component fluids comprising:
2 a plurality of heat exchange stages,
3 at least one scrubber adapted to receive at least one input liquid stream and at least one input
4 vapor stream and produce at least one output liquid stream and at least one output vapor stream, and
5 a plurality of mixers and splitters,
6 where the heat exchange stages and the at least one scrubber and the mixers and the splitter
7 are configured to form are interconnected in such a way that streams are split and mixed so that a
8 mixed partially condensed stream derived from a vapor multi-component feed stream for enters each
9 of the heat exchange stages, where each partially condensed stream has parameters adapted to
10 increase increasing a heat transfer coefficient in each of the heat exchange stages, where each of the
11 heat exchange stages is adapted to fully condense its partially condensed stream, and where a last
12 heat exchange stage is adapted to produce a fully condensed multi-component output stream.
- 1 2.(original) The apparatus of claim 1, where the plurality of heat exchange stages is two.
- 1 3.(original) The apparatus of claim 1, where the plurality of heat exchange stages is three.
- 1 4.(original) The apparatus of claim 1, where the plurality of heat exchange stages is four.
- 1 5.(original) The apparatus of claim 1, where the plurality of heat exchange stages is more than
2 four.
- 1 6.(currently amended) The apparatus of claim 1, further comprising a plurality of scrubbers,
2 where the scrubber plurality is equal to or one less than the plurality of heat exchanger exchange
3 stages.
- 1 7.(currently amended) The apparatus of claim 6, where the heat exchange stage plurality is
2 three and the scrubber plurality is two.

1 8.(original) The apparatus of claim 1, wherein the exchange stages are heat exchangers.

1 9.(currently amended) An apparatus for condensing multi-component fluids comprising:

2 a first plurality of heat exchange stages,

3 a second plurality of scrubbers adapted to receive at least one input liquid stream and at least
4 one input vapor stream and produce at least one output liquid stream and at least one output vapor
5 stream,

6 a third plurality of mixers, and

7 a fourth plurality of splitters,

8 where the ~~heat exchange stages and the scrubbers are interconnected in such a way that~~
9 streams are split and mixed so that a mixed stream enters each heat exchange stage increasing a heat
10 transfer coefficient in each of the heat exchange stages ~~the scrubbers, the mixers and the splitter are~~
11 configured to form a partially condensed stream derived from a vapor multi-component feed stream

12 for each of the heat exchange stages, where each partially condensed stream has parameters adapted

13 to increase a heat transfer coefficient in each of the heat exchange stages, where each of the heat

14 exchange stages are adapted to fully condense its partially condensed stream, and where a last heat

15 exchange stage is adapted to produce a fully condensed multi-component output stream.

1 10.(currently amended) The apparatus of claim 9, where the plurality of heat exchange stages
2 is two.

1 11.(currently amended) The apparatus of claim 9, where the plurality of heat exchange stages
2 is three.

1 12.(currently amended) The apparatus of claim 9, where the plurality of heat exchange stages
2 is four.

1 13.(currently amended) The apparatus of claim 9, where the plurality of heat exchange stages
2 is more than four.

1 14.(currently amended) The apparatus of claim 9, further comprising a plurality of scrubbers,
2 where the scrubber plurality is equal to or one less than the plurality of heat ~~exchanger~~ exchange

3 stages.

1 15.(currently amended) The apparatus of claim 614, where the heat exchange stage plurality
2 is three and the scrubber plurality is two.

1 16.(currently amended) The apparatus of claim 19, wherein the exchange stages are heat
2 exchangers.

1 17.(currently amended) A process for condensing multi-component fluids comprising the steps
2 of:

3 ————— feeding an input vapor stream comprising a multi-component fluid to a condensation system
4 of claims 1-16;

5 splitting the an input multi-component vapor stream into first and second vapor sub-streams;
6 forwarding the first vapor sub-stream to a lower port of a scrubber;
7 combining the second vapor sub-stream with a first scrubber liquid stream from a bottom
8 port of the scrubber to form a first mixed stream;

9 passing the first mixed stream through a first heat exchanger where it is fully condensed
10 forming a first condensed stream;

11 splitting the first a condensed stream into first and second condensed sub-streams, where the
12 condensed stream is the first condensed stream;

13 combining the second condensed sub-stream with a first scrubber vapor stream from an
14 upper port of the first scrubber to form a second mixed stream;

15 forwarding the first condensed sub-stream to a top port of a the scrubber;
16 counterflow compositionally equilibrating the first vapor sub-stream and the first condensed
17 sub-stream in the scrubber, and

18 passing the second combined mixed stream through a second heat exchanger where it is fully
19 condensed forming final liquid to form a fully condensed multi-component output stream, where
20 comprising a multi-component stream the fully condensed multi-component output stream has
21 having a compositions the same or substantially the same composition as the input multi-component
22 vapor stream,

23 where the streams entering each heat exchanger are mixed streams having a composition
24 designed to increase, optimize or maximize a heat transfer coefficient in each heat exchanger.

1 18.(currently amended) The process of claim 17, further comprising the steps of:
2 before the second splitting step, combining the first condensed stream with a second scrubber
3 vapor stream from a port in a middle section of the scrubber to form a third mixed stream,
4 passing the third mixed stream through a third heat exchanger where it is fully condensed
5 forming a second condensed stream, where the condensed stream is the second condensed stream.

1 19.(currently amended) The process of claim 17, further comprising the steps of:
2 before the second splitting step, splitting the first condensed stream into third and forth
3 condensed sub-streams,
4 forwarding the forth condensed sub-stream to a first port in a middle section of the scrubber;
5 combining the third condensed sub-stream with a second scrubber vapor stream from a
6 second port in the middle section of the scrubber above the first middle port to form a third mixed
7 stream,
8 passing the third mixed stream through a third heat exchanger where it is fully condensed
9 forming a second condensed stream, where the condensed stream is the second condensed stream.

1 20.(currently amended) The process of claim 17, further comprising the steps of:
2 before the second splitting step, combining the first condensed stream into with a second
3 scrubber liquid stream from a first port in a middle section of the scrubber to form a third combined
4 stream,
5 combining the third combined stream with a second scrubber vapor stream from another a
6 second port in the middle section of the scrubber above the first middle port to form a third mixed
7 stream,
8 passing the third mixed stream through a third heat exchanger where it is fully condensed
9 forming a second condensed stream, where the condensed stream is the second condensed stream.

1 21.(currently amended) A process for condensing multi-component fluids comprising the steps
2 of:
3 —— feeding an input vapor stream comprising a multi-component fluid to a condensation system
4 of claims 1-16;
5 splitting the an input multi-component vapor stream into first and second vapor sub-streams;

6 forwarding the first vapor sub-stream to a lower port of a first scrubber;
7 combining the second vapor sub-stream with a first scrubber liquid stream from a bottom
8 port of a second scrubber to form a first mixed stream;
9 passing the first mixed stream through a first heat exchanger where it is fully condensed
10 forming a first condensed stream;
11 combining the first condensed stream with a first scrubber vapor stream from a port in a
12 middle section of the first scrubber to form a second mixed stream,
13 passing the second mixed stream through a second heat exchanger where it is fully
14 condensed forming a second condensed stream
15 splitting the second condensed stream into first and second condensed sub-streams;
16 combining the second condensed sub-stream with a second scrubber vapor stream from an
17 upper port of the second scrubber to form a third mixed stream;
18 forwarding the first condensed sub-stream to a top port of the first scrubber;
19 forwarding a second scrubber liquid stream from a bottom port of the first scrubber to a top
20 port of the second scrubber,
21 forwarding a third scrubber vapor stream from an upper port of the first scrubber to a lower
22 port of the second scrubber,
23 counterflow compositionally equilibrating the first vapor sub-stream and the first condensed
24 sub-stream in the first scrubber,
25 counterflow compositionally equilibrating the second scrubber liquid stream and the third
26 scrubber vapor stream in the second scrubber, and
27 passing the third mixed stream through a third heat exchanger where it is fully condensed
28 forming a final liquid stream comprising a multi-component stream having a compositions the same
29 or substantially the same as the input stream,
30 where the streams entering each heat exchanger are mixed streams having a composition
31 designed to increase, optimize or maximize a heat transfer coefficient in each heat exchanger.

1 22.(original) The process of claim 21, further comprising the steps of:

2 before the second splitting step, combining the first condensed stream with a second scrubber
3 vapor stream from a port in a middle section of the scrubber to form a third mixed stream,
4 passing the third mixed stream through a third heat exchanger where it is fully condensed
5 forming a second condensed stream.

1 23.(original) The process of claim 21, further comprising the steps of:

2 before the second splitting step, splitting the first condensed stream into third and forth
3 condensed sub-streams,

4 forwarding the forth condensed sub-stream to a port in a middle section of the scrubber;

5 combining the third condensed sub-stream with a second scrubber vapor stream from a port
6 in the middle section of the scrubber to form a third mixed stream,

7 passing the third mixed stream through a third heat exchanger where it is fully condensed
8 forming a second condensed stream.

1 24.(currently amended) The process of claim 21, further comprising the steps of:

2 before the second splitting step, combining the first condensed stream into with a second
3 scrubber liquid stream from a port in a middle section of the scrubber to form a third combined
4 stream,

5 combining the third combined stream with a second scrubber vapor stream from another port
6 in the middle section of the scrubber to form a third mixed stream,

7 passing the third mixed stream through a third heat exchanger where it is fully condensed
8 forming a second condensed stream.

1 25.(new) An apparatus for condensing multi-component fluids comprising:

2 a first splitter valve adapted to receive a multi-component vapor feed stream and to form a
3 first vapor feed sub-stream and a second vapor feed sub-stream,

4 a scrubber apparatus adapted to receive the first vapor feed sub-stream at a lower port and
5 a first portion of a first condensed stream in a top port and to produce a liquid scrubber stream at a
6 bottom port and a vapor scrubber stream at an upper port,

7 a first mixer valve adapted to combine the second vapor feed sub-stream and the liquid
8 scrubber stream to form a first combined stream,

9 a first heat exchange stage adapted to fully condense the first combined stream to form a first
10 condensed stream, where the first combined stream has parameters adapted to increase a heat
11 transfer coefficient of the first heat exchanger,

12 a second splitter valve adapted to divide the first condensed stream into two portions,
13 a second mixer valve adapted to combine a second portion of the first condensed stream and

14 the vapor scrubber stream to form a second combined stream,
15 a second heat exchanger adapted to fully condense the second combined stream to form a
16 fully condense multi-component output stream, where the second combined stream has parameters
17 adapted to increase a heat transfer coefficient of the second heat exchanger.

1 26.(new) The apparatus of claim 25, wherein the scrubber apparatus includes a single scrubber.

1 2827.(currently amended) The apparatus of claim 25, wherein the scrubber apparatus includes
2 two scrubbers.

28.(new) An apparatus for power generation comprising:

 a vaporization unit adapted to fully vaporize a fully condensed multi-component working fluid stream into a fully vaporized multi-component working fluid stream;

 an energy extraction unit adapted to convert a portion of thermal energy in the fully vaporized multi-component working fluid stream and to produce a spent multi-component working fluid stream,

 a condensation unit including:

 a plurality of heat exchange stages,

 at least one scrubber, and

 a plurality of mixers and splitters,

the at least one scrubber, the mixers and the splitter are configured to form a partially condensed stream derived from a vapor multi-component feed stream for each heat exchange stage, where each partially condensed stream has parameters adapted to increase a heat transfer coefficient in each of the heat exchange stages, where the heat exchange stages are adapted to fully condense its partially condensed stream, and where a last heat exchange stage is adapted to produce a fully condensed multi-component output stream.